

Alternatives for Carbon Dioxide Capture

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Abstract

Globally, the rising emissions of greenhouse gases (GHG) pose a serious problem for the environment and the general public. This rise is the result of rapidly expanding urban and industrial areas, where emissions of gases including carbon dioxide (CO_2), methane (CH_4), and nitrogen oxides (NO_x) are rising. A new approach called nanotechnology is being used extensively in many different energy systems. In recent years, there has been a lot of interest in the revolutionary method of CO_2 absorption or conversion increase employing nanofluids. This review paper attempts to review for research on various CO_2 absorption methods, CO_2 Capture increase by use of nanofluids is dealt in detail in this review. Effective Factors in the CO_2 Absorption by Nanofluid have also been discussed.

Key words : CO_2 capture, Nanofluids, Nanotechnology, Amines, GHG emissions,

1.0 Introduction :

The main causes of carbon dioxide (CO_2) emission are population expansion, economic development, and the use of fossil fuels in industrial and domestic transportation. Global warming and climate change are caused by the greenhouse gas effect, which is brought on by the direct release of created CO_2 into the atmosphere. Since industrial processes produce CO_2 , a lot of research should be done to offer a practical and effective way to make them clean and avoid the environmental issues linked with them. For this purpose, many researchers have proposed several processes, including amine-based absorption (Zhou et al., 2021), membrane (Jang et al., 2022), adsorption, cryogenics and chemical looping combustion for CO_2 capture. However there are many advantages and disadvantages of these various technologies. Even though there are lots of benefits of these technological approaches, their disadvantages convinced scientists to identify better ways for CO_2 capture.

2.0 Methods for CO₂ capture :

There are three basic types of CO₂ capture: 1.pre-combustion, 2.post-combustion and 3. Oxyfuel with post-combustion. Pre-combustion processes convert fuel into a gaseous mixture of hydrogen and CO₂. The hydrogen is separated and can be burnt without producing any CO₂; the CO₂ can then be compressed for transport and storage. Post-Combustion capture, where CO₂ is separated from flue gas after fossil fuel combustion. Oxy-fuel combustion capture, where pure oxygen is fed to combustion chamber instead of air to produce a flue gas of CO₂ and H₂O

Among the aforementioned technologies, Post-Combustion capture is typically the one that is employed the most. Using chemical, physical, or biological methods, this capture system separates CO₂ after burning (Wang et al., 2011). The most cutting-edge method of carbon capture at the moment is chemical absorption utilising aqueous amines. According to many researchers amines (primary, secondary, tertiary, and sterically hindered) make up the majority of the solvents utilised for chemical CO₂ absorption. According to Muchan et al. (2017), the alkanolamines in particular exhibit excellent capacity and selectivity for CO₂ absorption from various gas streams. Triethanolamine was the first amine solvent to be used commercially for gas purification (TEA). Primary amines such as monoethanolamine (MEA) and diglycolamine (DGA) were next, followed by secondary amines such as diethanolamine (DEA) and (DIPA), and tertiary amines such as methyldiethanolamine (MDEA).

2.1 Use of Ionic Liquids

The absorption of CO₂ has also been done using ionic liquids (ILs). According to Carvalho (2015), ILs are cation and anion salts that are liquid (at room temperature) and offer great solubility, thermal and chemical stability, and flexible structural adjustment. Due to their viscosity, ILs have a lower CO₂ solubility than alkanolamines, but they also require between 25 and 50 percent less energy to regenerate (Lian et al., 2021).

2.2 Adsorption :

Adsorption is a possible substitute for chemical absorption techniques that is currently being considered for extensive CCS applications. According to Varghese and Karanikolos (2020), the processes that produce the CO₂ adsorption capability are chemisorption (chemical adsorption) and physisorption (physical adsorption). Zeolites, carbons, silica, alumina, Metal Organic Frameworks (MOFs), and Zeolite Imidazolate Frameworks (ZIFs) are the major materials that exhibit physical sorption, although surface-functionalized adsorbents exhibit chemisorption to a lesser extent. In comparison to absorption, adsorption has a lesser uptake capacity (on a volume or weight basis). Adsorption uses less energy than

other processes Due to a stronger chemical interaction between the solvent and CO₂ and a greater temperature required for regeneration in the latter, the cost of regeneration is nearly 90% lower than chemical absorption by amines (Wang 2015).

2.3 Use of Membranes:

According to size and/or diffusion affinity, membranes are reasonably priced semipermeable sheets that can separate gases (Lee et al., 2019). Polymeric, inorganic, and mixed matrix membranes, among others, are used for carbon capture (Muthukumaraswamy Rangaraj et al., 2020,). Other recently established methods for CO₂ capture include biological and photochemical conversion (Yaashikaa et al., 2019), and mineralization of waste water (Dindi et al., 2018). Although less developed and still being evaluated for large-scale applications, several technologies show promising future.

2.4 Hybrid Systems :

Hybrid systems are being researched as a way to improve carbon capture efficiency overall by combining the advantages of adsorption and absorption. These systems consist of distributed and suspended solid adsorbents in liquid solvents. Due to improved heat and mass transfer and CO₂ solubility, these devices may effectively extract carbon dioxide from flue and other gas combinations while requiring less energy for sorption and regeneration. However, phase stability, material and energy costs, pumping challenges, and solvent reactivity pose challenges to the performance of hybrid systems. With regard to optimum setup and operation, the slurry hybrid system for carbon capture may ultimately be a promising In recent years, The CO₂ is captured by the hybrid systems through both adsorption and absorption processes.solution for the industrial scrubbing process.

2.5 Nanofluids for CO₂ Capture :

Recently, absorption-based techniques to absorb carbon dioxide (CO₂) molecules have been used using nanofluids. The ability of nanofluids to absorb CO₂ is influenced by pressure, temperature, the kind and concentration of nanoparticles in the host liquid, and the length of gas-liquid contact. In order to maximise overall uptake and energy savings, slurry (nanofluid) systems combine the adsorption and absorption capacities of carbon dioxide (Yu et al., 2019).

Small amounts of nanoscale solid adsorbent are dispersed in a liquid solvent during the preparation of these hybrid systems using one- or two-step procedures . Additionally, many researchers have suggested that dispersing nanoparticles in a base fluid is a useful way to effectively capture CO₂ molecules . Methanol-based (Kim et al., 2014; Torres Pineda et al., 2012), monoethanolamine-based (Jiang et al., 2014), methyl diethanolamine-based (Jiang et al., 2014; Zhou et al., 2021), and water-based (Golkhar

2013) processes have all been experimentally tried using nanofluids. (**Rashidi and Mamivand, 2022; Rashidi et al., 2013; Mehdipour et al., 2021**) The most commonly used nanosized additives to these base liquids are carbon nanotubes (CNT), multi-walled CNN, graphene oxide, SiO₂, TiO₂, MgO, ZnO, Al₂O₃, and carbon nanotube (CNT) **Golkhar et al., 2013; Jiang et al., 2014; Kim et al., 2014; Mehdipour et al., 2021; Torres Pineda et al., 2012; Zhou et al., 2021**).on the CO₂ removal by nanofluids. In comparison to values seen with pure amine solvents, nanofluids have been demonstrated to improve CO₂ uptake by over 20% and the CO₂ capture rate by 2–93%. The rate of CO₂ desorption can be greatly accelerated by nanoparticles with catalytic effects on CO₂ capture by up to 4000%.

When utilising nanoparticles in the form of nanofluids in bubbling absorption systems for CO₂ capture, **Ganapathy et al.2013** discovered gas-liquid absorption augmentation that varied for each kind of nanoparticle. In a gas-liquid absorption system, the gas concentration in the liquid phase slightly rises until equilibrium is established In a study, **Fang et al. 2016** investigated the impact of nanoparticles on CO₂ absorption using a bubbling ammonia system. The effectiveness of CO₂ capture and the type of nanoparticle were shown to be related. TiO₂ > CuO > SiO₂ was the order of CO₂ capture efficiency **Sumin et al. 2013** investigated the effectiveness of CO₂ removal in a stirred reactor comprising CNT and Al₂O₃ nanoparticles. The outcomes of their research showed a significantly improved CO₂ collection.when using carbon nanotubes in the absorption solvent .

A new annular contactor (AC) that made use of a tray absorber was the subject of a study by **Pineda et al.2014** that examined the effects of adding TiO₂, SiO₂, and Al₂O₃ nanoparticles to the absorption solvent. This study indicated that adding TiO₂, SiO₂, and Al₂O₃ nanoparticles, respectively, might increase absorption rates by up to 5%, 6%, and 10% . In their studies, **Zhang et al. 2016** used a stirred reactor to study the impacts of particle size and optimal nanoparticle concentration as well as the effects of TiO₂ nanoparticle addition into propylene carbonate on the system's capture rate. **Golkhar et al.2013** removed CO₂ using a nanofluid including carbon nanotubes and silica nanoparticles in a gas-liquid hollow fibre membrane contactor. Their findings showed that CNT nanofluid has better performance in CO₂ removal with up to 40% efficiency.

Numerous studies have revealed that the performance of gas absorption can be significantly improved by adding promoters or dispersing a third phase, such as solid particles (**Sumin, L.U et al .2013**) As a result, replacing amine solvents with amine-based nanoparticle absorbents that are dispersed in the liquid phase can result in large energy savings because these absorbents don't need a lot of energy for repeated heating and cooling cycles to recover the liquid solvent [**Arshadi et al 2019**].

Al₂O₃, SiO₂, and TiO₂ nanoparticle dispersions were employed by Wang et al. in MEA base fluid for CO₂ collection operations. The greatest improvement in CO₂ absorption was shown with TiO₂ [Wang et al 2016]. There are other reports like these in the literature. Jiang et al. 2013 conducted some studies to ascertain the impact of four SiO₂, MgO, TiO₂, and Al₂O₃ nanoparticles on the enhancement of CO₂ capture. Among the four solutions, they discovered that TiO₂-MDEA nanofluids have the best CO₂ absorption performance.

3.0 Effective Factors in the CO₂ Absorption by Nanofluid

The characteristics of nanofluids have created a new area for technological development. To be used as absorbents in CO₂ absorption processes, several nanofluids have been the subject of research. In this regard, a variety of metal oxide, metallic, and nonmetallic nanoparticles, including TiO₂, MgO, SiO₂, Cu, CuO, Al₂O₃, and carbon nanotubes, have been investigated for improving CO₂ absorption [Rahmat et al 2016]. The key variables were chosen based on the outcomes of CO₂ absorption by nanoparticles. These include the base fluid type, flow rate, pressure, temperature, and hydrodynamics as well as the nanoparticle type, shape, size, and concentration in the base fluid, gas flow rate, CO₂ concentration in the feed stream, and gas flow rate.

3.1 Effect of Nanoparticle Concentration

The influence of temperature and ZnO and SiO₂ nanoparticle concentration in a water-based nanofluid on CO₂ absorption was studied in one experiment using an isothermal quasi-static high pressure stirred reactor. The results showed that increasing temperature marginally decreases CO₂ absorption, however adding 0.1 weight percent ZnO and SiO₂ enhances CO₂ absorption by 14% and 7%, respectively Haghtalab, A. et al 2015. Nabipour et al. 2017 looked into the effects of adding MWCNTs to the CO₂ absorbent fluid, and the results showed that doing so increased the CO₂ equilibrium solubility by 23.2% when compared to the base fluid at a concentration of 0.02 weight percent of MWCNTs with carboxyl functional groups in the Sulfinol-M absorber.

Kim et al. 2008 tested CO₂ absorption in a bubble absorber system to assess the effectiveness of a nanofluid containing SiO₂ nanoparticles on CO₂ absorption. In comparison to pure water as its base fluid, the 0.21 weight percent nanofluid demonstrated a 24% improvement in CO₂ absorption performance. When 0.02 weight percent of Ag nanoparticles were added to the solution, the rate of CO₂ absorption rose by 55%, according to Peng et al. Lee and Kang 2013 employed a bubble column system to study the

effects of adding Al_2O_3 nanoparticles to a NaCl solution on the system's ability to absorb CO_2 and found that as little as 0.01 vol% of Al_2O_3 nanoparticles can increase the CO_2 solubility. All of these studies show that an absorption fluid's ability to absorb can be improved by adding tiny amounts of nanoparticles.

Recent research by **Darvanjooghi et al. [2018]** on the CO_2 absorption capacity of a nanofluid containing Fe_2O_3 nanoparticles revealed that the maximum mean CO_2 flow 105 mol/(m².s) was attained at a Fe_2O_3 concentration of 1 wt.%, which declined over time.

In their investigation of the impact of Al_2O_3 nanoparticles on the mass transfer of a water-based nanofluid, **Periasamy Manikandan et al.** discovered the greatest CO_2 absorption augmentation at 0.6 vol% Al_2O_3 nanoparticle concentration [95]. To test the effectiveness of a solution mixture of MEA, DEA, and diisopropanolamine in absorbing CO_2 in a stirred cell, **Huang et al.** and **Park et al. [2007,2008]** added SiO_2 nanoparticles to the solution. By increasing the concentration of nanoparticles, they observed a decrease in the CO_2 absorption rate, which is thought to be connected to the solution's elasticity [**Komati 2008**]. These studies show that the CO_2 absorption of a nanofluid is greatly improved by the addition of modest numbers of nanoparticles to the fluid.

Irani et al. 2019 evaluated the use of a graphene-Oxide/MDEA nanofluid mixture in the gas sweetening process. Because of the higher mass transfer coefficient brought on by the hydroxyl functional groups on the graphene oxide surface, adding just 0.1 weight percent of graphene oxide to the solvent might boost its absorption capacity by 9.1%. In a different investigation, **Park et al. 2006** examined the effects of colloidal nanosilica addition to the solvent 2-amino-2-methyl-1-propanol on the effectiveness of CO_2 absorption in a stirred vessel. They discovered that the absorption rate and the volumetric mass transfer coefficient in the liquid side decrease as the concentration of nanoparticles rises. Because DEA is a potent chemical CO_2 absorbent, **Rahmatmand et al. [2016]** have also shown that the addition of CNT nanoparticles has no discernible impact on the DEA absorption performance. However, CNTs could considerably improve the MDEA-based nanofluid's ability to absorb CO_2 . In general, it can be said that raising the concentration of nanoparticles in the base fluid enhances absorption capacity

3.2 Effect of Nanoparticle Size

Lot of research has also been done on effect of nanoparticle volume fraction. Al_2O_3 , SiO_2 , and TiO_2 nanoparticles, among many other types of nanoparticles, were used in studies of CO_2 mass transfer efficiency increase by the addition of nanoparticles to aqueous solutions [**Lee 2016, Said 2016**]. **Nagy et al. 2007** increased mass transfer by more than 200% by mixing 10 vol% of 65 nm-sized n-hexadecane nanoparticles into a fluid. The findings show that whereas the rate of mass transfer increases slowly at

greater particle concentrations (more than 6 vol%), it does so quickly at low nanoparticle concentrations. Smaller Al_2O_3 nanoparticles were added to a NaCl solution, and Lee and Kang came to the conclusion that this increased the fluid's ability to absorb CO_2 [Lee et al 2013].

According to a review of the literature, Kim et al 2008. were the only research team to examine how nanoparticles affect the efficiency of mass transfer in nanofluids. They mixed water with silica nanoparticles with average particle sizes of 30, 70, and 120 nm to create a nanofluid with a concentration of 0.021 weight percent. The absorption of CO_2 by a nanofluid containing 0.021 wt% nanoparticles was improved by up to 76%, with 24% of this improvement occurring in the first minute of the absorption process's eight-minute duration. The corresponding increases for nanofluids containing K_2CO_3 nanoparticles were 11% and 12%, respectively. Their analysis came to the conclusion that the presence of tiny bubbles in nanofluids enhanced mass transfer. According to Hwang et al.2009, the volumetric mass transfer coefficient improves until the particle size reaches 60 nm, beyond which it has no effect on the effectiveness of nanofluid CO_2 absorption. Increasing nanoparticle volume fraction tends to raise the enhancement factor while increasing nanoparticle size tends to lower it [Zhang, N et al 2014].

3.3 Effect of Temperature

Temperature is a significant factor in the enhancement of CO_2 absorption by nanofluids. A new CO_2 absorbent made of Al_2O_3 nanoparticles in a NaCl aqueous solution was developed by Lee and Kan 2013. In this nanofluid, they tested the solubility of CO_2 at various temperatures and Al_2O_3 concentrations. At 30 °C, 20 °C, and 10 °C, respectively, they achieved 11%, 12.5%, and 8.7% augmentation in CO_2 capture when Al_2O_3 nanoparticle concentration was 0.01 vol% in the solution. Another study by Lee et al.2013, conducted in a bubble reactor, showed that at 20 °C and an Al_2O_3 concentration of 0.01 vol%, the rate of CO_2 absorption increased by 4.5%; this enhancement increased to 5.6% when Al_2O_3 was replaced by SiO_2 nanoparticles at the same temperature. At 0.01% Al_2O_3 nanoparticle concentration and 10 °C, Jung et al.2012 increased the rate of CO_2 absorption by 8% in a bubble reactor. These findings suggest that higher mass transfer efficiencies were obtained at lower nanoparticle concentrations.

4.0 Classification of Nanofluids Based on Base Liquid

Another difficulty is choosing the best solvent for CO_2 absorption. A good solvent needs to be readily available, inexpensive, non-toxic, corrosive, and combustible with a low vapour pressure. The most popular solvents for this purpose are brine, water, ionic liquids, amines, alcohols, amines, and piperazine (PZ) [Lin et al 2014]. The following introduces three different kinds of nanofluids: methanol, amines, and water mixes.

4.1 Amine-Based Nanofluid

Amine absorption of CO₂ is seen as a chemical process in which a mass transfer between the gaseous and liquid phases takes place. For this, absorption and desorption columns are employed. The absorption capacity of the chosen amine is determined by the gas-liquid equilibrium [Mandal, B et al 2001]. Amines absorb CO₂ with quick kinetics. The amino groups in an aqueous solution enhance alkalinity while the hydroxyl functional group in the amine increases water solubility and lowers vapour pressure [108]. As a result, the most popular solvent utilised in industrial gas sweetening procedures in scrubbers is aqueous alkanolamine solutions.

The classification of amines into three groups—primary amines like MEA, secondary amines like DEA, and tertiary amines like MDEA—is typically based on how many hydrogen atoms of an ammonia molecule are substituted with other functional groups [Hafizi et al 2020]. Secondary amines react quickly with acidic gases like CO₂ and have a higher rate of regeneration energy consumption than tertiary amines. The primary amine of MEA, which is highly reactive and practical from an economic standpoint, is the amine solvent utilised in large plants the most frequently. However, this solvent is aggressive and needs a lot of energy to regenerate. When nanofluids were utilised as the enhancing agent, Komati et al 2008. were able to increase the rate of absorption of CO₂ capture by amine solutions. They claimed that adding 0.39 vol% of nanoparticles to the base fluid increases its absorption capacity by 92.8% compared to the base fluid. The CO₂ absorption has been investigated using three base liquids (water, amine, and methanol). Water has captured more interest among researchers as a base liquid than the two other base liquids due to availability and being cheaper.

5.0 Future Perspective of nanofluids for CO₂ Capture :

Currently, hybrid systems can take the place of conventional procedures because of their effectiveness for CO₂ absorption. On the other hand, hybrid systems, due to their novelty, need additional research to comprehend the impact of parameters, the performance of nanomaterials, and analysis of the process to attain an ideal rate of absorption. Blockage, phase stability, a lack of data on solvent qualities, pump power, the expense of solid materials, an increase in heat and energy transfer, and the imposition of additional investment expenditures are a few of the difficulties associated with adopting hybrid systems. In this regard, in addition to accelerating mass transfer and enhancing gas-phase absorption by solid particles, two energy and economic difficulties in these systems can be managed by appropriately choosing nanoparticles and base liquid. In general, by analysing the interaction between mechanisms and carrying out thorough research on the role of nanofluids in CO₂ absorption, a hopeful viewpoint might be anticipated in the future

and at large sizes. Future research will focus further on CO₂ removal and absorption processes employing nanoparticles and other techniques.

Conclusion

In this study, we have investigated various methods for CO₂ absorption, application of hybrid systems, and their wide application in CO₂ absorption. Accordingly, we can conclude that such technology provides one of the effective solutions for CO₂ absorption. In this review study, the main focus is given on the use of nanofluid & its application for the CO₂ absorption. From this review, we can conclude that CO₂ absorption using nanofluids depends on several factors, i.e., particle size, nanoparticle type, temperature, and base liquid. The CO₂ absorption in the nanofluid depends on the different surfaces of the nanoparticles; as a nanoparticle has a larger surface, it is dispersed better in the base liquid, increasing the absorption level. There are different nanoparticles with particular applications and properties, but among them, making use of the metal oxide nanoparticles, e.g., Fe₃O₄, ZnO, Al₂O₃, TiO₂, CuO etc., have captured significant interest in industrial applications due to being cheaper. In general, according to the research conducted in the realm of mass transfer and CO₂ absorption so far, we can conclude that using nanofluids is an effective method for increasing the CO₂ absorption in terms of the base liquid that can decrease the energy consumption and equipment costs. With consideration of setup and operation circumstances, hybrid systems are an alluring under-investigation technique that could replace conventional processes. They still require further research to improve their performance and comprehend key factors because they are not yet fully developed.

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